

Pre - Feasibility Report on Silica Sand

Process Technology Developed

by

iNDEXTb

in association with
INDIAN BUREAU OF MINES
Government of India

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SALIENT DATA OF THE BENEFICIATION PROJECT

1. PLANT LIFE (MINIMUM) : 15 YEARS
2. PLANT CAPACITY : 100 M.T.P.D.
(2 SHIFT BASIS) 30,000 M.T.P.Y.
3. PLANT AVAILABILITY : 300 DAYS
4. PRODUCTION SILICA SAND: 75 M.T.P.D.
22,000 M.T.P.Y.(APPR.)
5. FEED GRADE : SiO₂ : 94.14%
Fe₂O₃: 0.45%
6. CONCENTRATE GRADE : SiO₂ : 99.40%
(-)~~30~~+120 # Fe₂O₃: 0.044%
7. WT% YIELD : 75.0
8. PROCESS : ATTRITION SCRUBBING,
CLASSIFICATION, ROD
MILLING, WET HIGH INTENSITY
MAGNETIC SEPARATION,
ROTARY SCREENING.
9. CAPITAL INVESTMENT : 2.75 CRORES
10. OPERATING COST : RS. 190/-/TONNE ORE MILLED,
RS.250/-/TONNE CONC. -
PRODUCED.

PART-I: BENEFICIATION

SECTION I: PROCESS DESCRIPTION:

The following is the brief description of the processing concept:

1.1 ORE HANDLING AND STOCK PILE:

The Run of Mine Ore would be transported and stock piled near the Beneficiation Plant.

The stockpiled ore will be delivered to the fine ore bin through a belt conveyor, having tramp magnet over it.

The feeder will draw the material at controlled rates from the bin and feed the same, through a conveyor to the attrition scrubber.

The ancillary equipment and facilities will include dry automatic sampler, weightometer, dust collecting system/ventilation etc.

1.2 CONCENTRATION:

From ore bin, the ore will be drawn through a feeder at controlled rate and through a conveyor fed to the wet attrition scrubber. The wet scrubbed product would be fed to the spiral classifier. The classifier overflow, containing the clayey material and constituting the 'Reject-I' would be pumped to the tailing/reject pond/area. The classifier underflow, through a classifier, would be pushed to the rod mill, for its milling. The Rod milled product, through a pump, would be fed to the wet High Intensity Magnetic Separator. The Magnetic fraction, constituting Reject-II would be pushed to the tailing pond/reject area. The Non-magnetic fraction, through a pump, would be passed to the circular vibrating screen, which would deliver the final desired product(s).

1.3 PROCESS FLOWSHEET:

The Flow diagram and flowsheet alongwith material balance of the Beneficiation Plant are given as Annexures I, II & III.

SECTION 2: PLANT DESIGN CRITERIA

PLANT LIFE - YEARS (MIN.)	:	15
NUMBER OF WORKING DAYS/YEAR	:	300
NUMBER OF OPERATING SHIFTS/DAY	:	2
NUMBER OF OPERATING HOURS/SHIFT	:	8
PLANT AVAILABILITY %	:	90
ACTUAL NUMBER OF WORKING HOURS	:	14-15
DESIGN DAILY MILLING (MTPD) RATE	:	100
DESIGN HOURLY MILLING (MTPH) RATE	:	7
SPECIFIC GRAVITY OF ORE SAMPLE	:	2.9
MILL HEAD GRADE - SiO ₂	:	94.14
CONCENTRATE GRADE ((-)30+120) SiO ₂	:	99.40
WT% YIELD	:	75.0
SILICA SAND CONC. PRODUCTION PER DAY (AVERAGE) - MTPD	} :	75

SECTION 3: CONCEPTUAL MASSFLOW BALANCE:

3.1 GENERAL:

This section contains details of conceptual Mass Flow balance for the various circuits of the concentration section.

The data is provided as an indication of the likely flow rates to occur under normal operating conditions. In practice slight fluctuations around these levels may be anticipated.

3.2 MASS FLOW BALANCE:

The mass flow balance of the various circuits of the concentration section is presented in Table No.1. The overall water balance is presented in Table No.7.

TABLE NO.1
MASS FLOW BALANCE

Sl.No	Product	Dry Wt Tonnes/hr	Water M ³ /hr	Pulp Tonnes/hr	% Solids	Wt% yield
1.	Feed to Scrubber	7.00	15.151	22.151	31.6	100.0
2.	Feed to classifier	7.00	18.521	25.521	27.0	100.0
3.	Classifier O/F	0.589	12.110	12.699	4.6	8.4
4.	Classifier U/F	6.411	6.411	12.822	50.0	91.6
5.	Feed to Rod Mill	6.411	6.411	12.822	50.0	91.6
6.	Rod Mill discharge	6.411	6.411	12.822	50.0	91.6
7.	Feed to WHIMS	6.411	63.273	69.684	9.2	91.6
8.	Magnetic fraction	0.510	8.960	9.470	5.4	7.3
9.	Non-magnetic fraction	5.901	54.313	60.214	9.8	84.3
10.	Feed to vibrating screen	5.901	54.313	60.214	9.8	84.3
11.	Sieve analysis of Non-mag:					
	-30+80 mesh	4.431	2.797	7.228	61.3	63.3
	-80+100 mesh	0.441	1.044	1.485	29.7	6.3
	-100+120 mesh	0.392	1.186	1.578	24.8	5.6
	-120 mesh	0.637	49.286	49.923	1.3	9.1

SECTION 4: MAJOR PLANT MACHINERY

The major machinery for the Beneficiation plant would include:

1.	BELT CONVEYOR(S):		
	(i) for conveying stockpiled ore to fine ore bin	:	1 No.
	(ii) for conveying ore from ore feeder to attrition scrubber	:	1 No.
	(iii) for conveying classifier underflow to Rod Mill	:	1 No.
2.	ORE BIN	:	1 No.
3.	BELT FEEDER	:	1 No.
4.	ATTRITION SCRUBBER	:	1 No.
5.	SPIRAL CLASSIFIER (SIMPLEX)	:	1 No.
6.	ROD MILL	:	1 No.
7.	MAGNETIC SEPARATOR (ERIEZ)	:	1 No.
8.	VIBRATING SCREEN CIRCULAR	:	1 No.
9.	PUMPS	:	18 Nos.
	(i) OPERATING : 9 Nos		
	(ii) STANDBY : 9 Nos		

The details of Plant machinery/equipment are presented in Table No.2.

TABLE NO.2
LIST OF MAJOR EQUIPMENT/MACHINERY

Sl.No	Equipment/ machinery	Qty. No(s)	Make	Size	H.P.	Price (Appr.) Rs./lakhs
1.	Belt conveyor (for conveying stockpiled ore to F.O.B.)	1	Local	450/400 MM width L:20 MM (Approx.)	5	6.00
2.	Weigh Feeder	1	Local	Matching	-	1.00
3.	Ore bin	1	Local	2.18M x 4.36M x 6.54M	-	2.00
4.	Belt feeder (variable speed)	1	Local (Denver type)	Matching	1	2.00
5.	Belt conveyor (for conveying ore from belt ore feeder to attrition scrubber)	1	Local	375/450 M	5	6.00
6.	Attrition scrubber	1	Local	L 2.5M W 0.8 M H 2.0 M	20	12.00
7.	Spiral classifier (Simplex)	1	Local	1800MM/75MM RPM ADJUSTABLE	20	10.00
8.	Belt conveyor (for conveying C & U.F. to Rod Mill	1	Local	375/450MM	5	6.00
9.	Rod Mill	1	Local	1500 MM x 2400 MM	75	25.00
10.	Magnetic separator (Ericz Type: Model CF-100)	1	Local	Industrial Model	5	15.00
11.	Vibrating screen circular	1	Pennwalt	Standard	10	20.00
12.	Pumps	18	Local (Denver Type)	150 x 150MM: 4 Nos 125 x 125MM: 4 Nos 75 x 75MM: 2 Nos 50 x 50MM: 4 Nos 30 x 25MM: 4 Nos	10 10 10 4 2	20.00
				TOTAL	182	125.00

PART-II : COST ESTIMATION

SECTION 5: CAPITAL COSTS:**5.1 BASIS OF COSTS:**

The costs of major machinery/equipment are based on the prevailed price as per reputed manufacturers of the country. The estimates for erection, piping, chutes, electricals, civils/structures are made on percentage basis of the equipment cost as are generally applicable for such plants.

Costs for land acquisition and development, mining and transportation, infrastructure facilities etc. are excluded from the purview of the report.

Interest on fixed capital and working capital is not taken into account as this will depend on the capital phasing of the overall project and the equity/debt ratio.

5.2 CAPITAL COST ESTIMATE:

The details of machinery/equipment costs, capital costs and capital investment are given in Table Nos. 2,3 & 4.

**TABLE NO.3
CAPITAL COST ESTIMATE**

		Rs. (lakhs)
1.	Fixed capital cost	250.00
2.	Working capital (10% of 1)	25.00
	Capital Investment:	275.00

**TABLE NO.4
CAPITAL COST DETAILS**

		Rs. (lakhs)
1.	Major equipment/machinery	125.00
2.	Installation: Erection, piping, chutes, electricals, civil (50% of 1)	63.00
3.	Miscellaneous/contingencies (15% of 1)	19.00
4.	Tailing Pond (10% of 1)	13.00
5.	Plant building (20% 1)	25.00
	TOTAL	245.00
	Say	250.00

SECTION 6: OPERATING COSTS:**6.1 BASIS OF COSTS:**

The cost of mining and delivery of the ore upto the Processing Plant is not included.

The power cost is based on the unit rates as prevalent for the industrial use and taken @ Rs. 3/- per KWH. The rates of water are taken as per its industrial use @ Rs. 5/- per kilolitre.

The estimated power cost is for the operation of major machinery/equipment in the plant. Care has been taken, by safety factor, for lighting.

The water requirements have been calculated for processing plant. Recirculation of water, after its recovery, has been taken care of. The requirement of personnel has been calculated and their wages taken as prevalent currently.

Depreciation at a uniform rate of 5% is taken.

6.2 OPERATING COST ESTIMATE:

The operating cost works out to be Rs. 190/- per tonne of ore milled/treated and Rs. 250/- tonne of finished product produced. The operating costs are presented in Table No.5. The details of operating cost are presented in Table No.6.

TABLE NO.5
OPERATING COST ESTIMATE

A. DIRECT OPERATING COST:

		Amount (Rs./Tonne milled)
i.	Electricity	66.00
ii.	Water	25.00
iii.	Grinding Media/Milling ore & other misc. items	10.00
iv.	Ore/Concentrate Handling	5.00
v.	Royalty	1.00
		107.00

B. FIXED OPERATING COST:

i.	Labour & Overheads	50.00
ii.	Maintenance shares	10.00
iii.	Depreciation (5%)	10.00
iv.	Internal services	10.00
v.	Plant Insurance (1%)	1.00
		81.00
	Total cost of Milling ore (A+B)	188.00
	The final cost of finished product (Silica sand conc.)	250.00

**TABLE NO.6
OPERATING COST DETAILS**

(I) MANPOWER:

Sl.No.	Manpower	No. of posts	Wages (Rs/month)	(Rs./Annum)
1.	Plant Manager	1	12,000	1,44,000
2.	Shift Incharge	3	24,000	2,88,000
3.	Mechanics	3	15,000	1,80,000
4.	Electricians	3	15,000	1,80,000
5.	PA to Manager	1	7,000	84,000
6.	Helpers	8	32,000	3,84,000
7.	Clerks	2	10,000	1,20,000
	Total	21		13,80,000

Labour Cost/Tonne milled: Rs. 46/-

(II) POWER:

TOTAL H.P. = 182

$$\frac{182 \times 0.746}{0.90 \times 7} = 21.55$$

Say 22 KWH/T ROM @ Rs. 3/-/KWT = Rs. 66/-/T Milled

TABLE NO. 7
WATER BALANCE

<u>Water in</u>	M ³ /hr
1. Water addition into Attrition scrubber	15.151
2. Water addition in feed to classifier	3.370
3. Water addition into Rod mill discharge	56.862

Total:	75.383

<u>Water out</u>	M ³ /hr
1. Classifier overflow (Reject I)	12.110
2. Magnetic fraction (Reject II)	8.960
3. -30 + 80 mesh fraction	2.797
4. -80 + 100 mesh fraction	1.044
5. -100 + 120 mesh fraction	1.186
6. -120 mesh fraction	49.286

	75.383

75% water can be reclaimed from the screen fractions i.e. $54.313 \times 0.75 = 40.734$

Therefore fresh water required/hr = $75.383 - 40.734$

$$= 34.649$$

or say 35 M³/hr

or say 280 M³/2 shift basis of -8 hours

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